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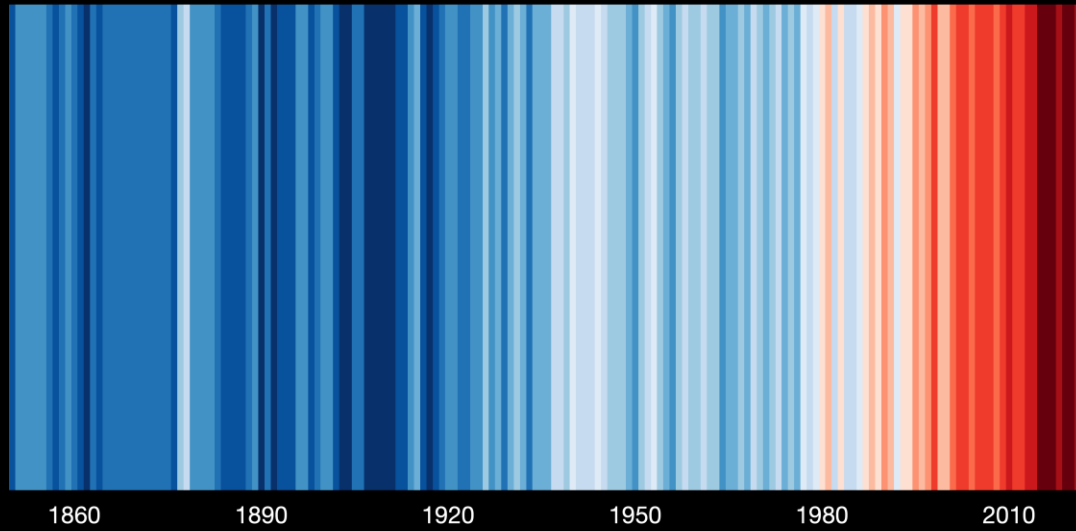
TURBINE DEPARTMENT  
CENTRE FOR HEAT AND POWER ENGINEERING

# ***COMPREHENSIVE ANALYSIS OF ORC-VCC SYSTEM FOR AIR CONDITIONING FROM LOW-TEMPERATURE WASTE HEAT***

ŁUKASZ WITANOWSKI

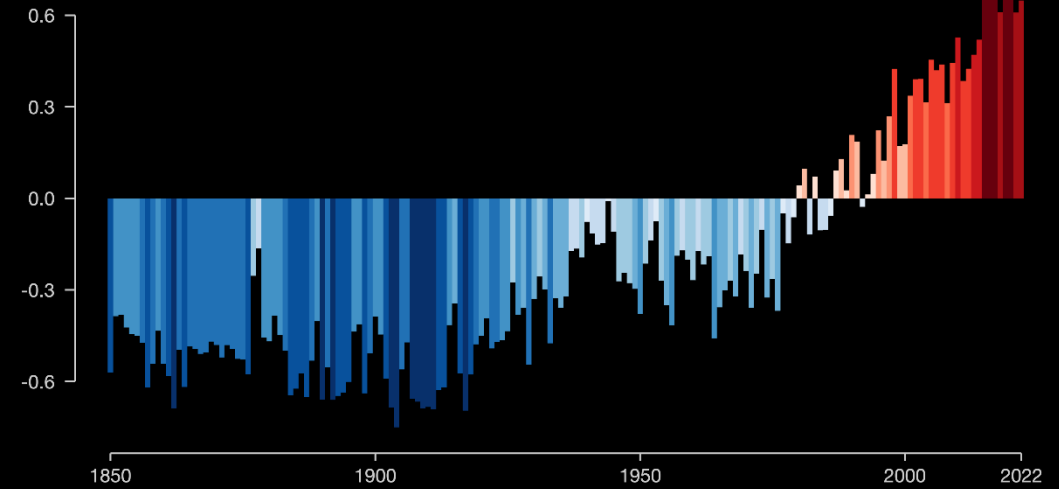
*Technical session 3B*  
**„Thermodynamics of ORC systems#1”**  
Chair: Piero Colonna

Global temperature change (1850-2022)

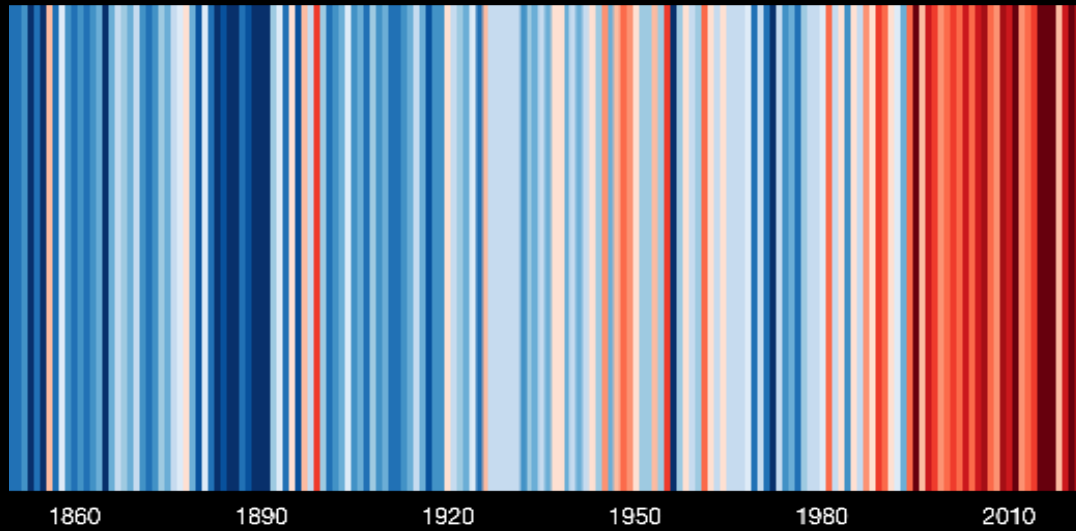


Global temperature change

Relative to average of 1971-2000 [°C]

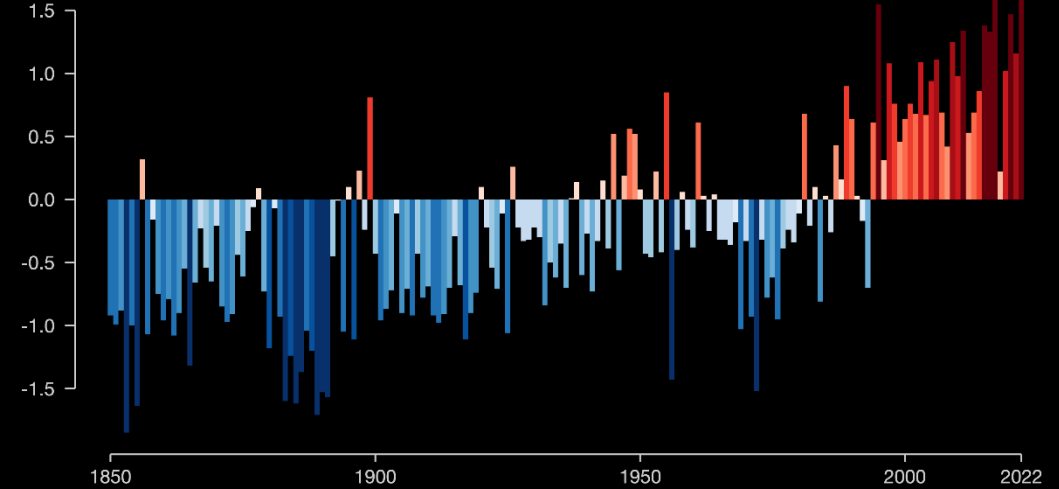


Temperature change in Sevilla since 1850



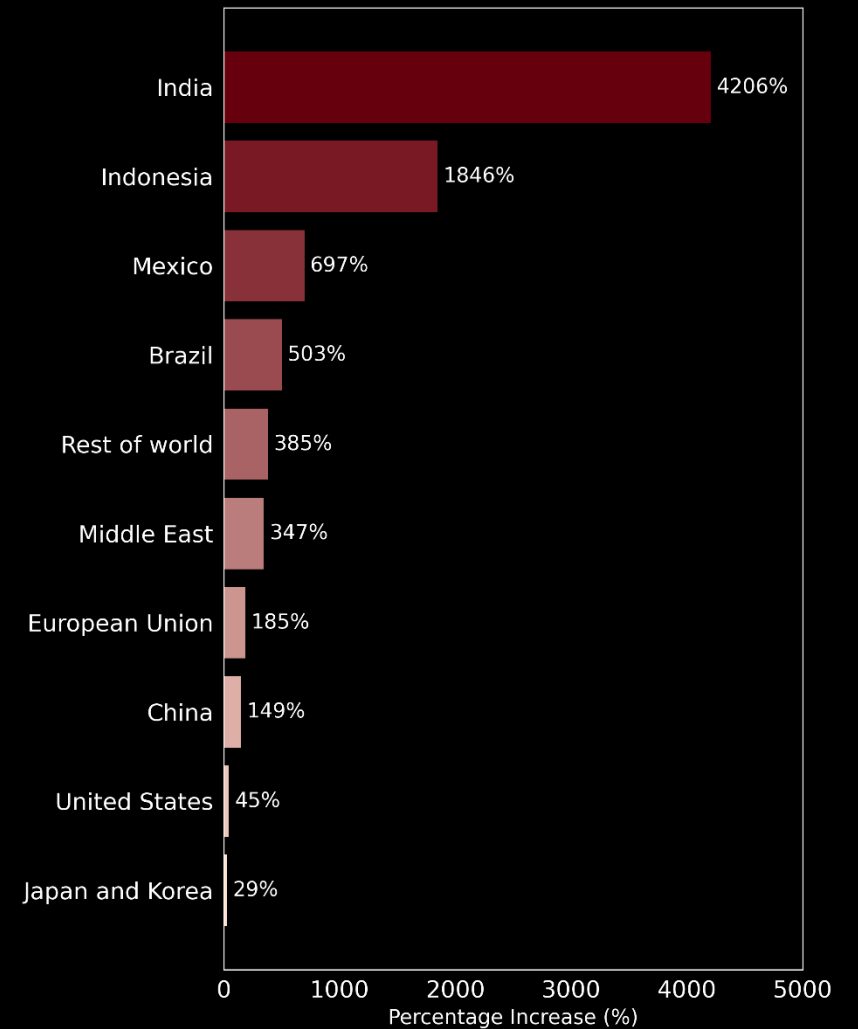
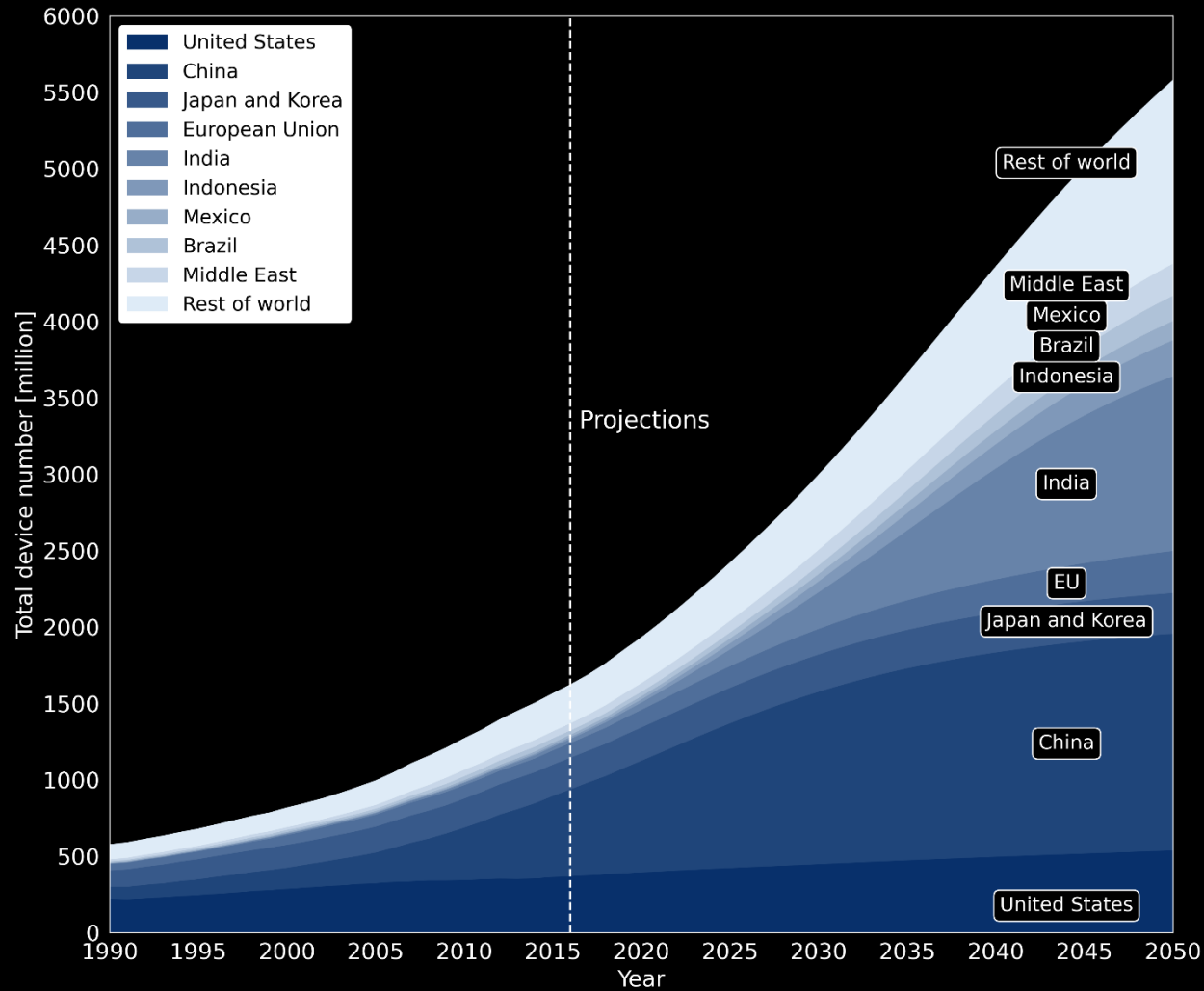
Temperature change in Sevilla

Relative to average of 1971-2000 [°C]



Graphics and lead scientist: Ed Hawkins, National Centre for Atmospheric Science, University of Reading., National Centre for Atmospheric Science, UoR.  
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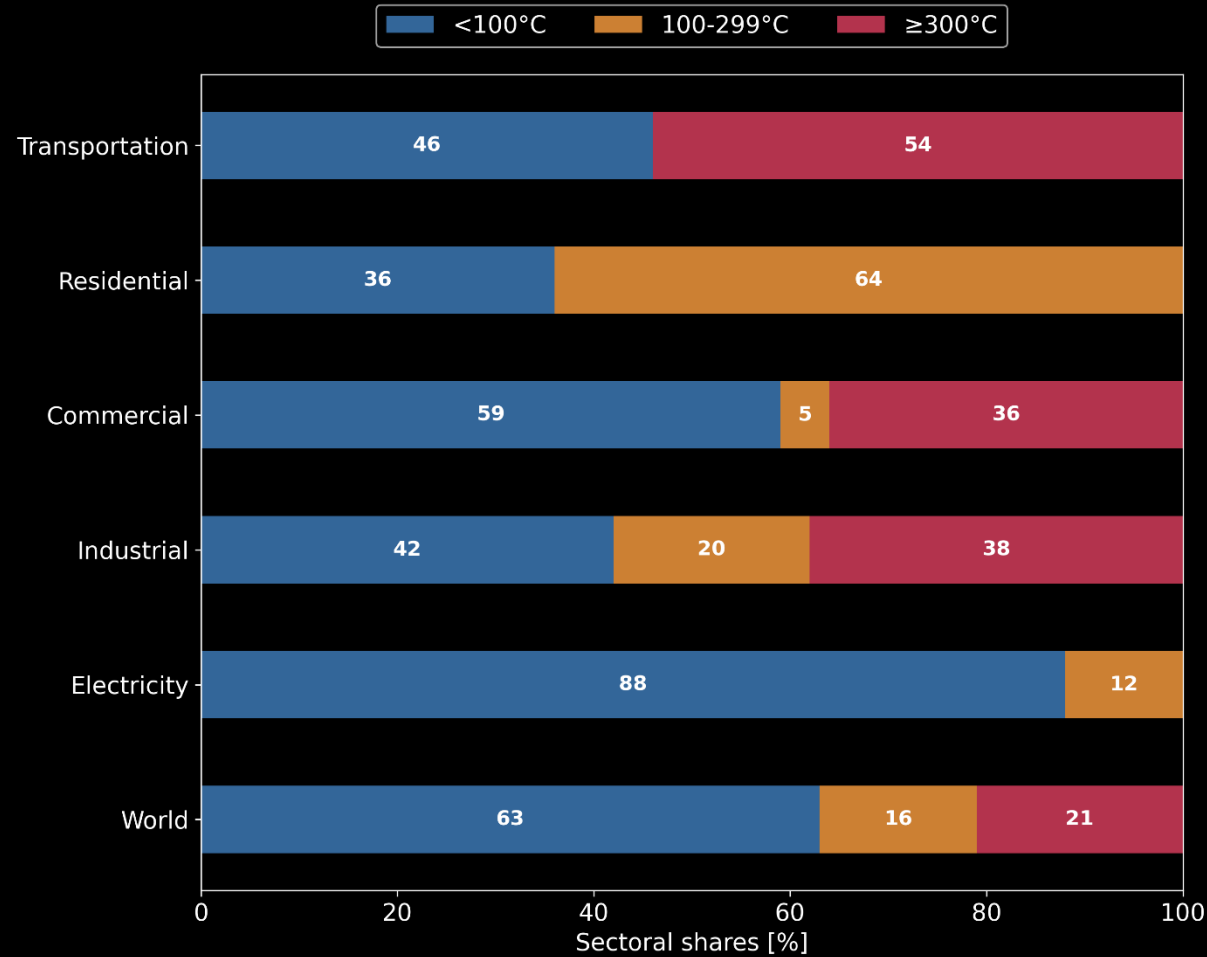
## Global air conditioner stock (1990-2050)



Source: IEA. This data is subject to the IEA's terms and conditions: [www.iea.org/t\\_c/termsandconditions](http://www.iea.org/t_c/termsandconditions) [2]

Graphics: Łukasz Witanowski

## Sectoral shares of waste heat distribution



### GLOBAL

- low temperature - 43.2 TWh
- medium temperature - 11.0 TWh
- high temperature - 14.1 TWh

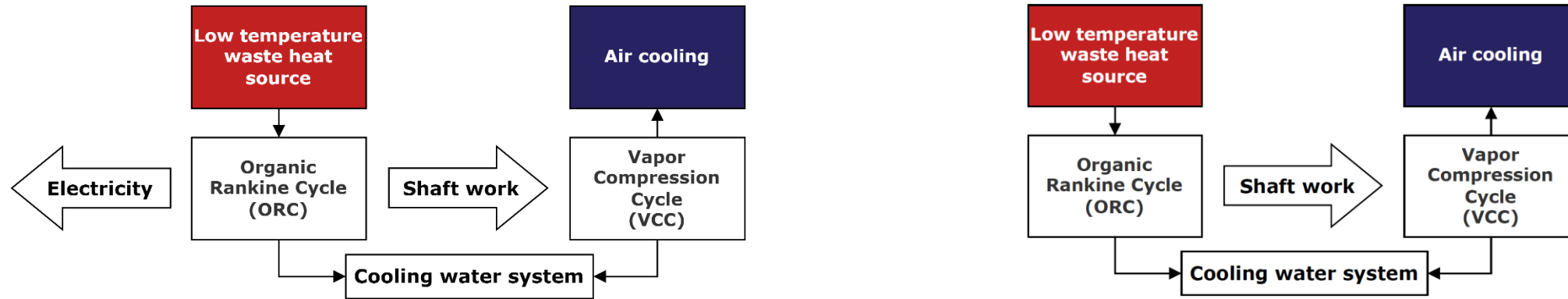
### INDUSTRIAL

- low temperature - 3.8 TWh
- medium temperature - 1.8 TWh
- high temperature - 3.4 TWh

### ELECTRICITY GENERATION

- low temperature - 26.2 TWh
- medium temperature - 3.6 TWh

TYPE	TECHNOLOGY READINESS LEVEL	ADVANTAGES	DISADVANTAGES	Ref.
<b>ABSORPTION SYSTEM</b>	System tests, <b>TRL9</b>	<ul style="list-style-type: none"> <li>• High efficiency.</li> <li>• Versatility of configurations.</li> </ul>	<ul style="list-style-type: none"> <li>• High investment costs.</li> <li>• Frequent maintenance required.</li> <li>• High operational costs.</li> <li>• Limited operating conditions.</li> <li>• Complex installation.</li> </ul>	[4]
<b>ADSORPTION SYSTEM</b>	System tests, <b>TRL9</b>	<ul style="list-style-type: none"> <li>• Low noise level.</li> </ul>	<ul style="list-style-type: none"> <li>• High investment costs.</li> <li>• Low efficiency.</li> </ul>	[5]
<b>EJECTOR SYSTEM</b>	System tests, <b>TRL9</b>	<ul style="list-style-type: none"> <li>• Simple construction.</li> <li>• Reliability.</li> <li>• Limited maintenance requirements.</li> <li>• Low investment and operational costs.</li> </ul>	<ul style="list-style-type: none"> <li>• Low efficiency.</li> <li>• Narrow operational characteristics.</li> <li>• High working pressure often required.</li> </ul>	[6]
<b>THERMOELECTRIC SYSTEM</b>	Technology development, <b>TRL4/TRL5</b>	<ul style="list-style-type: none"> <li>• Low failure rate.</li> <li>• Compact size and low weight.</li> <li>• Low levels of noise and vibration.</li> <li>• Precise temperature control.</li> </ul>	<ul style="list-style-type: none"> <li>• Low efficiency.</li> <li>• High investment costs.</li> <li>• High operational costs.</li> <li>• Limited applicability.</li> <li>• Legislation restricting the use of HFCs in small cooling devices.</li> </ul>	[7]
<b>MAGNETOCALORIC SYSTEM</b>	Technology development, <b>TRL4/TRL5</b>	<ul style="list-style-type: none"> <li>• Ability to adapt technology to specific needs.</li> <li>• Wide operational range.</li> </ul>	<ul style="list-style-type: none"> <li>• Low efficiency.</li> <li>• High investment costs.</li> <li>• High operational costs.</li> <li>• High electrical energy consumption.</li> </ul>	[8]
<b>ORC-VCC</b>	Research to prove feasibility, <b>TRL3/TRL4</b>	<ul style="list-style-type: none"> <li>• High efficiency across a wide operational range.</li> <li>• Low electrical energy consumption.</li> <li>• Low failure rate.</li> <li>• Low operational costs.</li> </ul>	<ul style="list-style-type: none"> <li>• Sensitivity to partial efficiencies of compressors and turbines.</li> </ul>	[9]



*Figure 1: Conception of the ORC-VCC systems.*

### Cooling and electricity generation

- Versatility.
- High efficiency of the system.

### Cooling generation

- High efficiency of the expander and compressor.
- High efficiency of the system.
- Wide operating characteristics of the system.
- Simplicity.

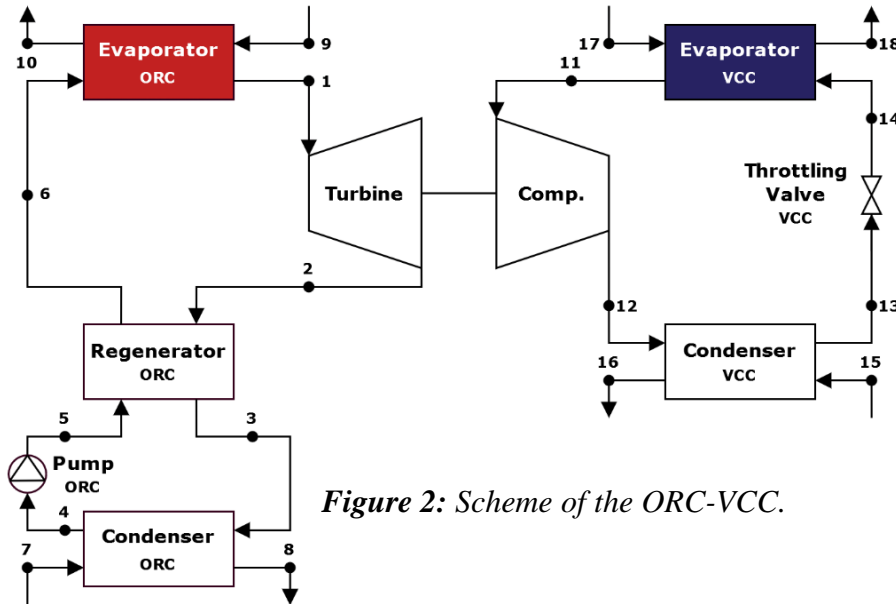


Figure 2: Scheme of the ORC-VCC.

## EFFICIENCY AND THERMODYNAMIC ASSUMPTIONS

- Chilled water temperature (cold side) – 8°C
- Chilled water temperature (hot side) – 12°C
- Cooling water temperature (cold side) – 15°C
- Heat source mass flow – 1 kg/s
- Heat source temperature (hot side) – 95°C
- Compressor efficiency – 80%
- Pump efficiency – 50%
- Turbine efficiency – 80%
- Pressure losses not included.
- $p_2 = p_{12}$  !
- R1224yd(Z), R1233zd(E), R133yd(Z).

## ECONOMICAL ASSUMPTIONS

- Electricity prices for non-household consumers [10]:
  - Greece 0.3042 €/kWh
  - Italy 0.2525 €/kWh
  - Poland 0.1555 €/kWh
  - Spain 0.1879 €/kWh
- Cost of ORC-VCC system (up to 35 kWth) – 30 000 €
- Discount rate (NPV analysis) – 5%
- Operation time – 8 years
- Annual operation time – 8000 h

1.  $C_i = (P_{comp} - P_{porc} - P_{pcs}) * AOT * C_{ei}$
2.  $SPBT = C_s / C_i$
3.  $NPV = \sum_{j=1}^t \frac{C_{ij}}{(1+d)^j} - C_s$
4.  $\sum_{j=1}^t \frac{C_{ij}}{(1+IRR)^j} = C_s$

## Optimization

„the act of making something as good as possible” (Cambridge Dictionary)



*Figure 3: Optimization concept.*



## OBJECTIVE FUNCTIONS

### R1233zd(E)

$$f_0 = NPV$$

$$f_1 = IRR$$

$$f_2 = \eta_{cyc}$$

$$f_3 = 0.3 \times NPV + 0.7 \times \eta_{cyc}$$

$$f_4 = 0.5 \times NPV + 0.5 \times \eta_{cyc}$$

$$f_5 = 0.7 \times NPV + 0.3 \times \eta_{cyc}$$

### R1336mzz(Z)

$$f_6 = NPV$$

$$f_7 = IRR$$

$$f_8 = \eta_{cyc}$$

### R1224yd(Z)

$$f_9 = NPV$$

$$f_{10} = IRR$$

$$f_{11} = \eta_{cyc}$$

## PENALTY FUNCTIONS

- Temperature.
- Mass flow rate.
- Turbine power > Compressor power

- Optimization algorithm – hybrid algorithm, Genetic Algorithm (GA) + Pattern Search Method (PA).
- MATLAB script.
- 11 parameters (decision variables).
- 8 penalty functions.

## PARAMETERS

- $x_1$  Evaporator pinch temperature difference (VCC)
- $x_2$  Degree of superheating in evaporator (VCC)
- $x_3$  Degree of subcooling in condenser (VCC)
- $x_4$  Regenerator pinch temperature difference (ORC)
- $x_5$  Degree of superheating in evaporator (ORC)
- $x_6$  Degree of subcooling in condenser (ORC)
- $x_7$  Evaporator pinch temperature difference (ORC)
- $x_8$  Condenser pinch temperature difference (ORC)
- $x_9$  Saturation temperature in evaporator (ORC)
- $x_{10}$  Saturation temperature in evaporator (ORC)
- $x_{11}$  Chilled water mass flow rate

UNIT	LB	UB
K	3	10
K	3	10
K	3	10
K	3	15
K	3	15
K	7	15
K	3	10
K	3	10
°C	50	85
°C	25	55
kg/s	0.7	2

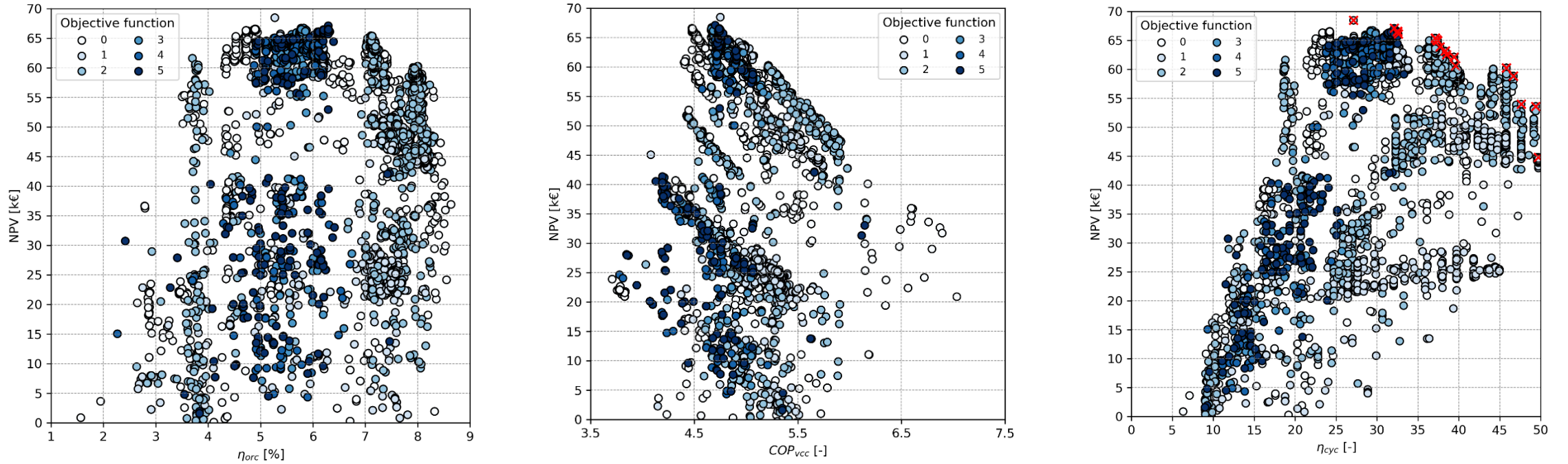
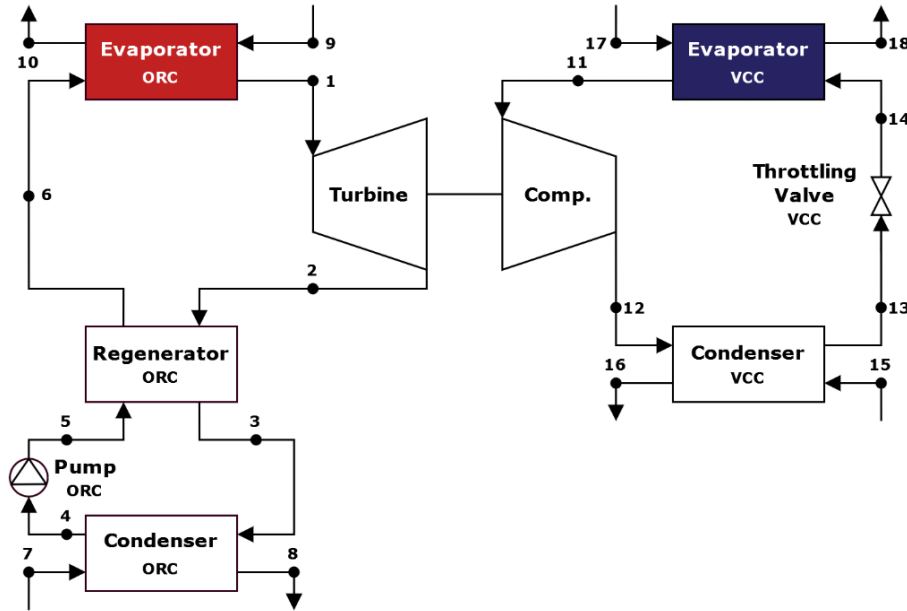


Figure 4: of NPV with  $\eta_{orc}$  (left),  $COP_{vcc}$  (center) and  $\eta_{cyc}$  (right).



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- $x_{10}$  Saturation temperature in evaporator (ORC)
- $x_{11}$  Chilled water mass flow rate

UNIT	LB	O	UB
K	3	9.82	10
K	3	5.24	10
K	3	9.28	10
K	3	13.97	15
K	3	4.65	15
K	7	8.38	15
K	3	5.81	10
K	3	4.17	10
°C	50	64.9	85
°C	25	41.26	55
kg/s	0.7	1.99	2

### ORC

$t_1 = 73.73^\circ\text{C}$ ,  $p_1 = 447 \text{ kPa}$   
 $t_2 = 55.06^\circ\text{C}$ ,  $p_2 = 210 \text{ kPa}$   
 $t_3 = 48.82^\circ\text{C}$ ,  $p_3 = 210 \text{ kPa}$   
 $t_4 = 34.61^\circ\text{C}$ ,  $p_4 = 210 \text{ kPa}$   
 $t_5 = 34.85^\circ\text{C}$ ,  $p_5 = 447 \text{ kPa}$   
 $t_6 = 79.19^\circ\text{C}$ ,  $p_6 = 447 \text{ kPa}$   
 $t_8 = 31.11^\circ\text{C}$ ,  $t_{10} = 65.62^\circ\text{C}$

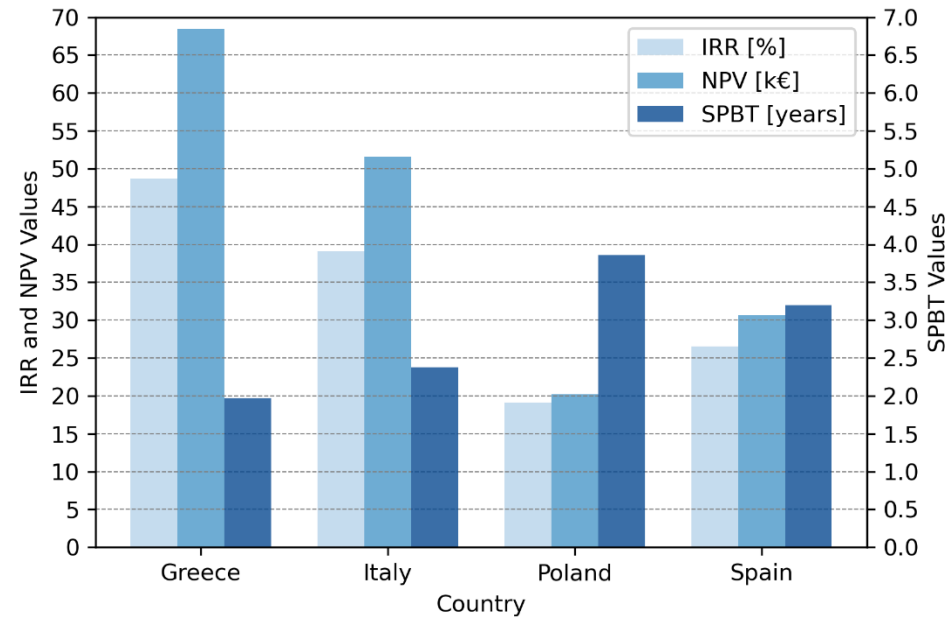
### VCC

$t_{11} = 3.41^\circ\text{C}$ ,  $p_{11} = 44 \text{ kPa}$   
 $t_{12} = 51.21^\circ\text{C}$ ,  $p_{12} = 210 \text{ kPa}$   
 $t_{13} = 29.97^\circ\text{C}$ ,  $p_{13} = 210 \text{ kPa}$   
 $t_{14} = -1.83^\circ\text{C}$ ,  $p_{14} = 44 \text{ kPa}$   
 $t_{16} = 31.11^\circ\text{C}$

$P_{\text{tur}} = 6.97 \text{ kW}$   
 $P_{\text{comp}} = 6.93 \text{ kW}$   
 $P_{\text{p\_orc}} = 0.23 \text{ kW}$   
 $P_{\text{p\_cs}} = 0.46 \text{ kW}$

$\text{IRR} = 48.65\%$   
 $\text{NPV} = 68.47\%$   
 $\text{SPBT} = 1.97$

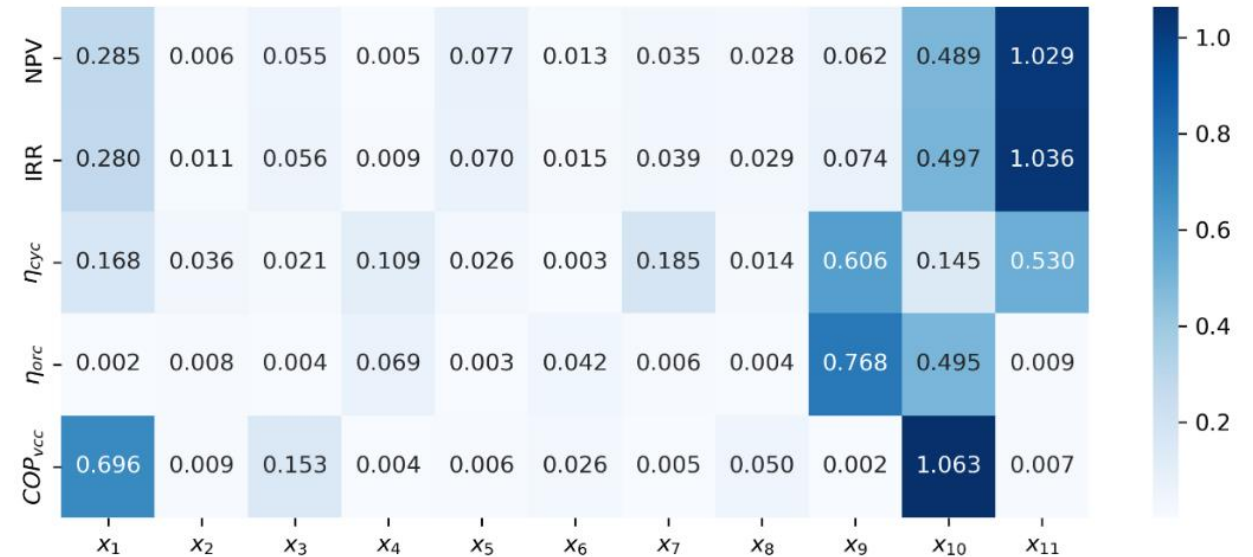
$\eta_{\text{cyc}} = 27.1\%$   
 $\eta_{\text{orc}} = 5.27\%$   
 $\text{COP}_{\text{vcc}} = 4.75$



*Figure 5: Comparison of economic indicators in selected UE countries.*

## PARAMETERS

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- $x_{11}$  Chilled water mass flow rate



## **ORC-VCC SYSTEM FOR AIR CONDITIONING**

Due to the need to reduce electricity consumption, methods of increasing the efficiency are being sought.

One of the possibilities is the use of low-temperature waste heat for electricity or/and cooling.

Simplified version of the system was investigated.

An in-house code was developed for cycle calculation.

Various novel working fluids are considered.

Single and multi-objective optimization was conducted.

The obtained cycle efficiency was 27.1%.

Simple pay back time was received less than 2 years.

- [1] [www.showyourstripes.info](http://www.showyourstripes.info), Ed Hawkins, National Centre for Atmospheric Science, University of Reading., National Centre for Atmospheric Science, UoR.
- [2] [www.iea.org/t\\_c/termsandconditions](http://www.iea.org/t_c/termsandconditions), The International Energy Agency.
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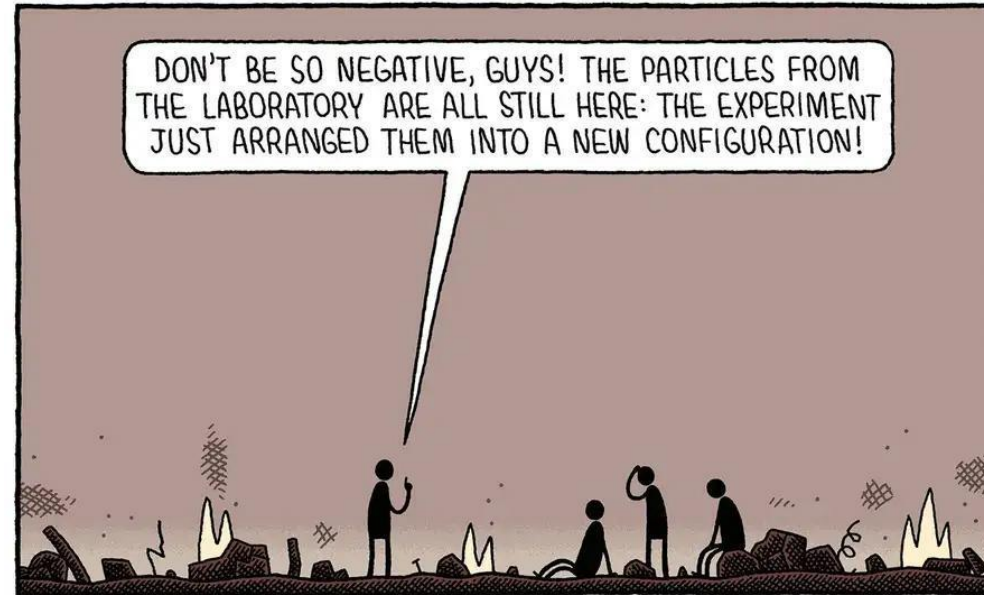


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lwitanowski@imp.gda.pl, witanowski@outlook.com

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